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# Fabrication of $Cu^0$ -composited $CuFe_2O_4$ magnetic nanoparticles on diatomite support for efficient degradation of tetracycline hydrochloride by a Fenton-like system

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# ABSTRACT

Paramagnetic Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composites were fabricated by a one-step solvothermal method to design a heterogeneous Fenton-like catalyst to degrade tetracycline hydrochloride (TC). The Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE were characterized by SEM, TEM, XRD, BET, and XPS methods. The catalytic activity of CuFe<sub>2</sub>O<sub>4</sub> was improved using diatomite and Cu<sup>0</sup>. Diatomite (DE) enhanced the dispersity of Cu/CuFe<sub>2</sub>O<sub>4</sub>, minimized metal ions leaching, and improved stability. The Cu<sup>0</sup> is used for the regeneration of Fe<sup>3+</sup>. The synergy between Cu<sup>+</sup>/Cu<sup>2+</sup> and Fe<sup>2+</sup>/Fe<sup>3+</sup> redox pairs promotes hydroxyl radical production upon H<sub>2</sub>O<sub>2</sub> decomposition. The synthesized materials were characterized by SEM, TEM, XRD, BET, and XPS, and their catalytic activities were discussed and analyzed. 95.5 % TC was degraded within 90 min (initial conditions, pH = 5.0 and [TC] 50 mg/L), and showing excellent anti-interference ability to the presence of SO<sub>4</sub><sup>2-</sup>, Cl<sup>-</sup>, NO<sub>3</sub>, CO<sub>3</sub><sup>2-</sup> and humic acid (HA). The presence of active species, viz., •OH and •O<sub>2</sub> radicals generated in the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub> system were detected by ESR quenching measurements. The •OH and •O<sub>2</sub> mediated TC degraded pathways were proposed using the intermediates identified by LC-MS data. The novel heterogeneous Fenton-like process developed using Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub> is robust for TC degradation as exemplified in its stability and reusability measurements.

# 1. Introduction

Antibiotics are widely used in medicine, animal husbandry, and agriculture posing a serious threat of their wastes to the environment [1]. Tetracycline (TC) is a widely used antibiotic in medical treatment and animal husbandry. It is persistent and stable under natural environmental conditions with a long half-life [2,3]. TC weakly absorbs by living organisms thus emanating it readily through wastes creating serious implications for ecosystem health [4–6]. In recent years, TC is frequently detected in surface water, drinking water, and soils at elevated proportions [7,8]. Although relatively low concentrations of TC are detected in the natural aqueous environment ( $\mu$ g/L-ng/L), high concentrations (100–500 mg/L) are detected in effluents of hospital and

pharmaceutical industries [9,10]. Therefore, the development of novel methods to remediate TC-polluted wastewater is a pressing global need.

Presently, TC in water is treated using adsorption [11], membrane separation [12], biodegradation [13], photocatalysis [14], and advanced oxidation processes [15]. Both adsorption and membrane separation methods concentrate TC without really destroying them. Biodegradation methods sometimes are not efficient to treat TC due to their microbial resistance [16]. Photocatalysis techniques are costly and time intensive especially in treating TC-laden wastewater [17]. When compared to these methods, the advanced oxidation processes (AOPs) are efficient as they completely destruct antibiotics via non-selective free radicals generated in different routes [18–20]. Among them, Fe<sup>2+</sup>/Fe<sup>3+</sup> in the traditional Fenton process can activate H<sub>2</sub>O<sub>2</sub> to

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generate highly reactive •OH destruct antibiotics into benign products [21]. Homogeneous Fenton oxidation has disadvantages such as slow reaction, narrow operational pH window [22], and excess iron-containing sludge production [23]. However, the heterogeneous Fenton-like processes can overcome these shortcomings; they have the advantages of simple operation, high efficiency, low cost, and less sludge production [24]. In heterogeneous Fenton-like catalysts, the presence of iron-containing compounds is mandatory. CuFe<sub>2</sub>O<sub>4</sub> with spinel structure is a P-type semiconductor material with a narrow band gap of 1.4 eV, which can respond under visible light without photo-corrosion [25]. CuFe<sub>2</sub>O<sub>4</sub> is chemically stable, environmentally benign, and easily recoverable under a magnetic flux. However, it has some inherent limitations such as sluggish electrons transfer for Fe<sup>3+</sup>  $\rightarrow$  Fe<sup>2+</sup> conversion and easy particulates agglomeration.

Several zero-valent metals (Fe<sup>0</sup>, Al<sup>0</sup>, and Cu<sup>0</sup>) are commonly employed for the degradation of organic pollutants in water [26–28]. Cu<sup>0</sup> activates H<sub>2</sub>O<sub>2</sub> for •OH production to degrade organic pollutants, mainly through the Cu<sup>2+</sup>/Cu<sup>+</sup> catalytic reduction cycle under acidic conditions [29]. Zhou et al. [30] found complete degradation of p-benzoic acid within 25 min in the Cu<sup>0</sup>/H<sub>2</sub>O<sub>2</sub> system at pH 3.0. Cu<sup>0</sup> undergoes uncontrolled oxidation in water irrespective of the presence of organic pollutants in the system. However, they passivate after repeated use. Mixed valence metals offer an alternative solution for the destruction of organic pollutants. The reactivity of Cu<sup>0</sup>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite is enhanced enabling the destruction of 4-chlorophenol into harmless products, and the degradation efficiency is 10.9 times or 7.3 times higher than that of employing discrete Cu<sup>0</sup> or Fe<sub>3</sub>O<sub>4</sub> nanoparticles [31] Therefore, the catalytic performance of CuFe<sub>2</sub>O<sub>4</sub> can be enhanced by introducing Cu<sup>0</sup> into the composite.

To minimize catalyst agglomeration, materials with uniform void structures and large specific surface areas, such as diatomite [32], polystyrene [33], chitosan [34] and polymeric filter materials [35] are chosen as the carriers. Diatomite is a  $SiO_2$  polymorph around 10–50  $\mu$ m size range found in natural environments. It has high porosity, high specific surface area, lightweight, strong adsorption capacity, and high chemical stability. In diatomite shells, silicon hydroxyl sites abut from the surface can capture metal ions readily thus inhibiting catalyst leaching. Therefore, diatomite is an ideal carrier to retain a catalyst in a well-dispersed manner with minimal metal ions leaching [36]. Zhu et al. [37]. prepared Ag<sub>3</sub>PO<sub>4</sub>/diatomite composites with a photocatalytic efficiency four-fold higher than that of pure Ag<sub>3</sub>PO<sub>4</sub>. due to the efficient separation of photogenerated electron-hole pairs. Tan et al. [32] synthesized porous magnetic catalyst CoFe<sub>2</sub>O<sub>4</sub>/diatomite (CFD) by citrate combustion method. The high surface area, better crystal dispersion, and abundant active sites make CFD better than CoFe<sub>2</sub>O<sub>4</sub> for the degradation of bisphenol A (BPA). The pseudo-first-order reaction rate constant of CoFe<sub>2</sub>O<sub>4</sub>/DE is over five times higher than that of pure CoFe<sub>2</sub>O<sub>4</sub>. Therefore, the introduction of diatomite can reduce the particulates' agglomeration providing free active sites to improve the catalytic activity and stability.

Presently, we fabricated Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE and associated composites by a one-step solvothermal method, and their performance was examined for the degradation of TC via a heterogeneous Fenton-like process. The effect of solution pH, matrix ions, and humic acid on the efficiency of TC degradation was also assessed. The mechanistic pathways of TC degradation were elucidated by LC-MS and electron spin resonance spectroscopic methods. The sustainability of the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE Fenton-like process was also examined by mimicking real-world experiments.

#### 2. Experiments

#### 2.1. Materials and chemicals

Diatomite was purchased from International Building Materials Environmental Protection Technology Co., Ltd PR China. Ferric chloride hexahydrate (FeCl<sub>3</sub>•6H<sub>2</sub>O), copper chloride dihydrate (CuCl<sub>2</sub>•2H<sub>2</sub>O), sodium acetate (CH<sub>3</sub>COONa), and ethylene glycol (EG) were purchased from Sinopharm Chemical Reagent Co., Ltd, PR China. Polyethylene glycol (PEG2000), hydrochloric acid (HCl), sodium hydroxide (NaOH), tert-butanol (TBA), p-benzoquinone (BQ), and tetracycline hydrochloride (TC) were purchased from Shanghai McLean Chemical Co., Ltd, PR China. The analytical grade chemical reagents and deionized water were used as received in all experiments.

# 2.2. Synthesis of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE and allied composites

Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composites were synthesized by a one-step solvothermal method. Firstly, 0.5 g diatomite was dispersed in 30 ml of ethylene glycol, and then 1.6 mmol CuCl<sub>2</sub>•2H<sub>2</sub>O and 3.2 mmol FeCl<sub>3</sub>•6H<sub>2</sub>O were co-dispersed in 30 ml of ethylene glycol. While stirring, the CuCl<sub>2</sub>•2H<sub>2</sub>O and FeCl<sub>3</sub>•6H<sub>2</sub>O solutions were added dropwise to the diatomite suspension, and then 0.75 g polyethylene glycol and 2.0 g sodium acetate were added respectively to form a homogeneous green solution. The uniform green solution thus received was loaded into 100 ml polytetrafluoroethylene lining and autoclaved at 200 °C for 12 h. After cooling to room temperature, the precipitate was magnetically separated, washed three times with absolute ethanol and deionized water, and vacuum dried at 60 °C for 10 h. (The molar ratio of Cu<sup>0</sup>, CuFe<sub>2</sub>O<sub>4</sub>, and diatomite is approximately 1.008:1:10.320). The synthesis of Cu/CuFe<sub>2</sub>O<sub>4</sub>, Cu<sup>0</sup>, and Cu/DE catalysts was prepared as described above without adding diatomite and FeCl<sub>3</sub>•6 H<sub>2</sub>O, respectively. CuFe<sub>2</sub>O<sub>4</sub> and CuFe<sub>2</sub>O<sub>4</sub>/DE were obtained by oxidizing Cu<sup>0</sup> in Cu/ CuFe<sub>2</sub>O<sub>4</sub> and Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE nanocomposites using FeCl<sub>3</sub> aqueous solution. The term catalyst implied either of the following substrates; Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE, CuFe<sub>2</sub>O<sub>4</sub>/DE, Cu/CuFe<sub>2</sub>O<sub>4</sub>, CuFe<sub>2</sub>O<sub>4</sub>, or Cu/DE.

#### 2.3. Catalyst characterization

The crystalline phase and purity of the fabricated substrates were tested using a rotating target X-ray diffractometer (XRD, Rigaku, Japan). The microscopic morphology, structure, and elemental composition were analyzed by scanning electron (SEM, Hitachi, Japan) and transmission electron (HRTEM, JEOL, Japan) microscopy equipped with Xray energy dispersive spectrometer (EDS). The surface functional groups of the samples were analyzed by Fourier transform infrared spectrometer (Thermo Nicolet, USA). The surface chemical properties of the materials and the changes in the valence of the elements before and after the experiments were studied by X-ray photoelectron spectroscopy (XPS, Thermo, USA). The specific surface area and pore size distribution of the samples were investigated by a BET analyzer (Autosorb-IQ3, USA). The concentration of metal ions during the reaction was measured by an atomic absorption spectrometer (AA800, Perkin Elmer, USA).

# 2.4. TC degradation

A typical TC degradation experiment was carried out in batch mode in the dark. 10 mg catalyst was added to 50 ml (50 mg/L) TC aqueous solution, and the initial pH was adjusted with 0.1 M HCl or 0.1 M NaOH, under stirring. The catalyst was added for 30 min to ensure that the sample reached adsorption-desorption equilibrium, and then a predefined concentration of  $H_2O_2$  is added. At given time intervals, 1.0 ml of the reaction solution was taken out and the catalyst was filtered with a 0.45 µm polyether sulfone membrane filter, followed by the addition of 0.5 ml of methanol as a quencher to stop the reaction. To determine the reusability of the catalyst, the used catalyst was collected, washed, and dried for use in subsequent experiments.

# 2.5. Analytical methods

The concentration of TC was measured by liquid chromatography using a C18 column (4.6  $\times~250$  mm) through a high-performance liquid

chromatograph (LC, Shimadzu LC-20A, Japan) and a UV detector with a wavelength of 355 nm. The mobile phase consisted of 20 % acetonitrile and 80 % 10 mM oxalic acid solution at a flow rate of 1.0 ml/min. Analysis of total organic carbon (TOC) was carried out using a TOC analyzer (multi-N/c3100, Germany) to evaluate the mineralization rate of TC. Electron spin resonance spectroscopy (ESR, Bruker, Germany) was used to detect the reactive radicals generated during the reaction. The Specific electronic spin resonance spectroscopy (ESR) analysis procedures are in supporting Materials text 1. The degradation intermediates generated during TC degradation were determined and analyzed by a liquid chromatogram-time-of-flight mass spectrometer (ACQUITY UPLC LCT Premier XE, USA) to explore the possible degradation routes.

# 3. Results and discussion

# 3.1. Characterization of the as-synthesized catalysts

As shown in Fig. 1. the morphology and microstructure of diatomite (DE), Cu/CuFe<sub>2</sub>O<sub>4</sub>, and Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composites were examined by high-resolution field emission scanning electron microscopy (FESEM). FESEM analysis shows that the particle sizes of individual diatomite range from  $10 \,\mu$  to  $50 \,\mu$ m. The disc shape diatomite surface shows a large array of pores that offers ideal locations to adhere Cu/CuFe<sub>2</sub>O<sub>4</sub>. In the absence of diatomite, Cu/CuFe<sub>2</sub>O<sub>4</sub> nanocomposites readily agglomerate (Fig. 1.b). As shown in Fig. 1(a), a large number of pores are distributed on the surface of disc-shaped diatomite, and they provide housing for Cu/CuFe<sub>2</sub>O<sub>4</sub> minimizing particulates agglomeration. Some Cu/ CuFe<sub>2</sub>O<sub>4</sub>/DE particulates entered into the pores improving the dispersion (Fig. 1.c). Well-resolved Cu/CuFe<sub>2</sub>O<sub>4</sub>-impregnated diatomite (Cu/ CuFe<sub>2</sub>O<sub>4</sub>/DE) provides enhanced catalytic reactivity. As shown in Fig. 1. (d), Cu, Fe, O, and Si on Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE show homogeneous distribution which further confirms Cu/CuFe<sub>2</sub>O<sub>4</sub> adherence on diatomite with some uniformity.

Further structural details and elements distribution of Cu/CuFe<sub>2</sub>O<sub>4</sub>/ DE samples were examined by transmission electron microscopy (TEM) and selected area electron diffraction (SAED). As shown in Fig. 2(a) and (b) Cu/CuFe<sub>2</sub>O<sub>4</sub> is evenly dispersed on the surface and in the pores of diatomite, Fig. 3(c) is the HRTEM image of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE, which clearly shows some fringes with a lattice spacing of 0.25 nm, 0.29 nm, and 0.48 nm correspond to the (311), (220) and (111) crystal planes of CuFe<sub>2</sub>O<sub>4</sub> respectively [38] . The lattice spacing of 0.21 nm matches the (111) crystal plane of Cu<sup>0</sup> [39]. Five diffraction rings can be observed in Fig. 2(d) of the selected electron diffraction pattern of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE, also corresponding to the typical crystal plane of CuFe<sub>2</sub>O<sub>4</sub> [40,41]. Therefore, HRTEM and SAED images further confirmed that the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite was successfully synthesized.

The crystal structure and crystallinity of diatomite, Cu/CuFe<sub>2</sub>O<sub>4</sub> and Cu/CuFe2O4/DE were investigated by X-ray diffraction. As shown in Fig. 3(a), the diffraction peaks of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE located at  $2\theta = 18.3^{\circ}$ , 30.2°, 35.5°, 37.2°, 43.2°, 53.6°, 57.1°, 62.7°, and 74.2° correspond to (111), (220), (311), (222), (400), (422), (511), (400) and (533) crystal planes of CuFe<sub>2</sub>O<sub>4</sub> respectively (JCPDS: 77-0010). In addition, the diffraction peaks detected at  $2\theta = 43.3^{\circ}$ ,  $50.4^{\circ}$  and  $74.1^{\circ}$  correspond to the (111), (200), and (220) crystal planes of Cu<sup>0</sup> (JCPDS : 85–1326). The diffraction peak of diatomite around  $2\theta=26.6^\circ$  corresponds to the (101) crystal plane of SiO<sub>2</sub> (JCPDS : 46–1045) [42]. The Scherrer formula was used to calculate the grain size of Cu<sup>0</sup> and CuFe<sub>2</sub>O<sub>4</sub>. The average grain size of Cu<sup>0</sup> and CuFe<sub>2</sub>O<sub>4</sub> in Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE was 32.761 nm and 13.457 nm, which is smaller than that of pure Cu<sup>0</sup> (43.832 nm) and CuFe<sub>2</sub>O<sub>4</sub> (22.981 nm). The diffraction patterns of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE samples combine the characteristic diffraction peaks of Cu, CuFe<sub>2</sub>O<sub>4</sub>, and diatomite. The spectral data further confirms the successful fabrication of CuFe2O4 on diatomite (designated as Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE).

Fig. 3(b) displays the FT-IR spectra of diatomite, Cu/CuFe<sub>2</sub>O<sub>4</sub>, and Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composites. The IR bands of Cu/CuFe<sub>2</sub>O<sub>4</sub> at 451.70 cm<sup>-1</sup> and 578.93 cm<sup>-1</sup> correspond to Cu-O and Fe-O stretching vibrations [43], respectively. The IR bands at 465.66 cm<sup>-1</sup> and 1093.57 cm<sup>-1</sup> are due to the asymmetric stretching vibration of Si–O–Si, and the band at 796.44 cm<sup>-1</sup> is attributed to the bending vibrations of Si–O–Al in diatomite [44]. The Al may associate as an impurity in diatomite. In addition, the IR bands at 1632.01 cm<sup>-1</sup> and 3436.02 cm<sup>-1</sup> correspond to the bending and stretching vibrations of H-O-H and -OH adsorbed water on diatomite, respectively [45].

Diatomite is an ideal carrier for catalysts due to its unique porous structure. As shown in Fig. 4(a), the N<sub>2</sub> adsorption-desorption curves of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE and DE both follow a typical IV curve, showing the H3 hysteresis loop, indicating a mesoporous structure. This structure is conducive to the enrichment and diffusion of pollutants into the active centers of the catalyst improving its efficiency [32]. The specific surface areas and pore sizes of Cu/CuFe<sub>2</sub>O<sub>4</sub>, Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE, and diatomite are (11.6 m<sup>2</sup>g<sup>-1</sup>, 57.2 m<sup>2</sup>g<sup>-1</sup>, and 20.1 m<sup>2</sup>g<sup>-1</sup>) and (3.78 nm, 4.89 nm, and 6.08 nm), respectively. Compared with diatomite without a catalyst, Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE has a larger specific surface area and narrower pore size, which determines that Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE has better adsorption and catalytic activity.

Fig. 5 shows the XPS survey spectrums for pristine and Cu/CuFe<sub>2</sub>O<sub>4</sub>/ DE after TC degradation by a Fenton-like process (viz. hereafter spent Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE). The XPS survey spectrums show the presence of five elements (Fig. S1), namely Cu, O, Si, and C in both composites, viz. pristine and spent Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE. The presence of surface-derived C is ascribed to the carbonization of ethylene glycol used as a solvent and the hydrocarbons present in the ambient air [46,47]. Fine spectral



Fig. 1. FESEM images of (a) diatomite, (b) Cu/CuFe<sub>2</sub>O<sub>4</sub>(c) Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite, (d) Element mapping of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite.



Fig. 2. TEM image (a) and (b), HRTEM image (c), and SAED pattern (d) of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite.



Fig. 3. The XRD patterns (a) and FT-IR spectra (b) of synthesized catalysts.



 $\label{eq:Fig. 4. N_2 adsorption-desorption isotherms (a) and pore size distribution plots (b) of Cu/CuFe_2O_4, diatomite, and Cu/CuFe_2O_4/DE composite.$ 



Fig. 5. XPS spectra of Cu 2p (a), Fe 2p (b), O 1 s (c), Si 2p (d) for Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite.

variations were obtained by deconvolving Cu2p, O1s, Fe2p, and Si2p spectral signatures. The Cu2p signal deconvolved into six peaks; the satellite peaks at 932.74 eV and 952.52 eV correspond to Cu<sup>0</sup> and the peaks at 940.13 eV, 943.65 eV, 935.01 eV, and 954.69 eV correspond to the presence of Cu<sup>2+</sup> [48–50]. When TC degraded by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE via a Fenton-like process, the % mole Cu<sup>0</sup> of the used catalyst decreased from 50.2 % to 38.7 % showing Cu<sup>0</sup>  $\rightarrow$  Cu<sup>2+</sup> conversion.

Similarly, in Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE (both pristine and spent) the iron occurs in Fe<sup>2+,</sup> and Fe<sup>3+</sup> valence states as shown by the Fe2p deconvoluted peaks at 711.02 eV and 724.74 eV, and 719.10 eV, respectively [51,52]. As the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE assisted Fenton-like process commences for TC degradation, the %mole of  $Fe^{2+}$  has increased from 52.6 % to 60.7 % showing  $Fe^{3+} \rightarrow Fe^{2+}$  reduction. The surface  $Fe^{3+}$  may also consume via Cu<sup>0</sup> oxidation. However, the XPS spectral data shown here is not adequate to isolate these two processes. The O1s spectrum of the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite shows two peaks corresponding to lattice-bound O (530.48 eV) and surface hydroxyls (532.36 eV) which act as a nucleus in generating hydroxyl radicals required for a Fenton-like process [53]. The % mole composition of lattice O has decreased from 26.9 % to 15.4 % and the percentage of OH component of indicating that hydroxylation occurred on the surface during the catalytic reaction [54]. The peak at 103 eV of the Si 2p corresponds to the Si-O bond which shows negligible variation in both composites [32] which implies the role of DE as catalyst support.

# 3.2. Fenton-like catalytic activity of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composites

The Fenton-like performance of the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE was examined against Cu/DE, CuFe<sub>2</sub>O<sub>4</sub>/DE, CuFe<sub>2</sub>O<sub>4</sub>, and Cu/CuFe<sub>2</sub>O<sub>4</sub> measuring TC degradation efficiency. As shown in Fig. 6(a), when H<sub>2</sub>O<sub>2</sub> is added in the absence of a catalyst, the TC content in the reaction system does not change significantly with the contact time, indicating that H<sub>2</sub>O<sub>2</sub> oxidation has negligible TC degradation. In the presence of the catalyst, the TC degradation efficiency approximates 100 % within 90 min, showing

that Cu/CuFe $_2O_4$ /DE has a marked activation effect on H $_2O_2$ .

The Fenton-like effect of the substrates, e.g., CuFe<sub>2</sub>O<sub>4</sub>, CuFe<sub>2</sub>O<sub>4</sub>/DE, Cu/CuFe2O4, Cu/DE, Cu/CuFe2O4, and Cu/CuFe2O4/DE and H2O2 on the TC degradation was also examined (Fig. 6.b). Before evaluating the catalytic properties of the catalysts, the TC adsorption experiments were performed in the dark (shown in Fig. S2). The adsorption equilibriums of the catalysts were reached in about 30 min. The efficiency of TC degradation depends on the type of catalyst used. When CuFe<sub>2</sub>O<sub>4</sub>/H<sub>2</sub>O<sub>2</sub> was used less than 30 % TC degraded or removed from the solution. The CuFe<sub>2</sub>O<sub>4</sub> coagulate readily thus reducing its electron shuttling efficiency. When Cu/DE/H<sub>2</sub>O<sub>2</sub> is used, the degree of TC degradation is increased to about 50 % due to the activation of  $\rm Cu^0/\rm Cu^+/\rm Cu^{2+}$  redox sites for electron exchange (Fig. 6.b). Interestingly, when Cu/CuFe<sub>2</sub>O<sub>4</sub>/ H<sub>2</sub>O<sub>2</sub> is used, the TC degradation rate is enhanced significantly. The  $Cu^+/Cu^{2+}$  and  $Fe^{2+}/Fe^{3+}$  redox states on  $Cu/CuFe_2O_4$  promote electron transfer with H<sub>2</sub>O<sub>2</sub> for the production of hydroxyl radicals, resulting in over 85 % TC degradation. However, the coagulation of Cu/CuFe<sub>2</sub>O<sub>4</sub> particulates hinders the efficiency of the Fenton-like process. In contrast, when the Cu/CuFe<sub>2</sub>O<sub>4</sub> are dispersed on DE, particulates agglomeration is reduced significantly as exemplified by enhanced TC degradation rate, viz. over 95 % with Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE and H<sub>2</sub>O<sub>2</sub>.

As shown in Fig. S3, the catalytic performance of the Cu/CuFe<sub>2</sub>O<sub>4</sub>/ DE was enhanced with the amount of diatomite used. At a given mass of the catalyst when diatomite content is increased beyond 0.7 g, the catalyst activity is somewhat reduced due to the dilution of the active sites.

The effect of  $H_2O_2$  concentration on the degradation of TC was also investigated (Fig. 6.c). The rate of TC degradation by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE increases exponentially with the [H<sub>2</sub>O<sub>2</sub>] at a given catalyst concentration reaching an optimal when [H<sub>2</sub>O<sub>2</sub>] > 4 mM. This points to the saturation of surface sites with the H<sub>2</sub>O<sub>2</sub>. The solution pH also exerts a marked effect showing the highest TC degradation by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE at acidic conditions (pH < 3). When solution pH increases the TC degradation efficiency shows a marked reduction due to the rapid



**Fig. 6.** (a) Effect of different reaction systems on the degradation rate of TC; (b) Effect of different catalysts on the degradation rate of TC; (c) Effect of different  $H_2O_2$  dosages on the degradation rate of TC; (d) Effect of initial pH on TC degradation in the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub> system. (Reaction conditions: pH 5.0; initial TC, 50 mg/L; catalyst, 200 mg/L; H<sub>2</sub>O<sub>2</sub>, 4.0 mM).

conversion of Fe<sup>2+</sup> and Fe<sup>3+</sup> into iron oxyhydroxides, thus passivating the catalyst (Fig. 6.d) [55,56]. As pH increases the H<sub>2</sub>O<sub>2</sub> undergoes spontaneous decomposition which further inhibits the free radical production required for TC degradation [57]. Furthermore, the adsorption of TC by Cu/CuFe<sub>2</sub>O<sub>4</sub> under different pH conditions was also investigated. The zeta potential of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE was measured by a zeta potentiometer. As shown in Fig S4, the pHzpc of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is 7.12. When the pH of the solution is lower than 7.12, the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is positively charged and when the pH is greater than 7.12, the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is negatively charged. In the pH range of 3.3–7.7, TC behaves as a zwitterionic form, and in the range of pH below 3.3, TC is cationic species [58]. When the pH of the reaction system is 3, the positively charged Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE and the cationic form of TC repel each other due to electrostatic interaction, and the adsorption of TC by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE decreases but still maintains excellent TC removal rates. Therefore, the removal of TC in the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE + H<sub>2</sub>O<sub>2</sub>



**Fig. 7.** (a) The effect of common anions on TC degradation in Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE system; (b) The effect of HA on TC degradation in Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE system. (Reaction conditions: pH 5.0; initial TC, 50 mg/L; catalyst, 200 mg/L; H<sub>2</sub>O<sub>2</sub>, 4.0 mM).

reaction system is mainly attributed to the catalytic degradation process.

Natural water and wastewater contain a variety of ions and other solutes that exert an impact on the performance of Fenton-like catalysts [59]. The effect of Cl<sup>-</sup>, SO<sub>4</sub><sup>2-</sup>, NO<sub>3</sub>, CO<sub>3</sub><sup>2-</sup>, and natural organic matter on the degradation of TC by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub> was examined. As shown in Fig. 7(a), in the presence of CO<sub>3</sub><sup>2-</sup>, the degradation efficiency of TC decreased significantly due to its competing effect with TC for •OH capturing [60]. On the other hand, SO<sub>4</sub><sup>2-</sup> reacts with •OH forming reactive new free radicals [61], therefore the presence of SO<sub>4</sub><sup>2-</sup> promotes the efficiency of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE However, the presence of Cl<sup>-</sup> or NO<sub>3</sub> in solution exerts a negligible role in TC degradation. Therefore, the activity of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE sustains at a steady state despite the contrasting behavior of various solute species present in free radicals' production.

Humic acid fractions (HA), e.g., 30–50 % of total organic matter are ubiquitous in water [62]. As shown in Fig. S5, when [HA] < 40 mg/L, the TC degradation rate increases slightly with the [HA] thus promoting Fe<sup>3+</sup>  $\rightarrow$  Fe<sup>2+</sup> conversion [63]. HA usually has a high density of oxygen-containing functional groups and can be used in electron shuttling and metal ions complexing, improving the electron transfer efficiency and oxidation process [64]. HA recombines with iron ions to form complexes that reduce the redox potential between Fe<sup>3+</sup>/Fe<sup>2+</sup> cycles, thus promoting the conversion of Fe<sup>3+</sup> $\rightarrow$  Fe<sup>2+</sup> [65]. When the [HA] > 40 mg/L, the TC degradation efficiency decreases significantly with the [HA], as it can absorb Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE by poisoning the catalyst. Further, HA and TC compete for •OH resulting apparent reduction of the TC degradation efficiency.

The effect of the initial [TC] concentration as a function of its degradation by  $Cu/CuFe_2O_4/DE/H_2O_2$  was examined as shown in Fig. S5. As the [TC] increases its degradation efficiency is reduced significantly due to the limited availability of active sites on Cu/CuFe\_2O\_4/DE and the scavenging of free radicals by intermediate products (Fig. S5). During the experiment, we also conducted degradation tests on other kinds of antibiotic pollutants (sulfamethoxazole, oxytetracycline), and found that Cu/CuFe\_2O\_4/DE also had excellent catalytic degradation performance, the experimental results are shown in Fig S6.

#### 3.3. Possible degradation pathways of TC

The intermediates of TC degradation by  $Cu/CuFe_2O_4/DE/H_2O_2$  system were determined by high-performance liquid chromatography-mass spectrometry (HPLC-MS) and 11 intermediates are identified as given in Table S1. Accordingly, as shown in Fig. 8, two routes for TC degradation by Cu/CuFe\_2O\_4/DE/H\_2O\_2 can be suggested.

In the Fenton-like process, the electron-rich double bonds, phenolic and amide groups in TC are easily attacked by the electrophilic •OH radicals [66]. For pathway I, the C=C bond reacts with •OH radical first, and then the double bond is opened to form hydroxyl and carbonyl groups, respectively, yielding P1 (m/z = 461) and P2 (m/z = 477) intermediates [67]. The dimethylamine group on P2 is further attacked by •OH, deamidated, while the ortho and para positions of the phenol ring are also attacked by •OH, forming ketones and P3 (m/z = 362)

intermediates [68]. Then, P4 (m/z = 280) was further dehydrated and oxidized by •OH. Under the action of •OH and •O<sub>2</sub>, P4 was degraded through ring opening and loss of functional groups to produce smaller organic molecules, P5 (m/z = 149) and P6 (m/z = 145) [69]. In pathway II, the benzene ring is first opened to generate P7 (m/z = 509) intermediate, the C=C bond is opened, P7 is degraded to P8 (m/z = 525), and P8 deamidation, dehydration, and hydroxyl group form P9 (m/z = 367) [70]. Subsequently, smaller organic molecules P10 (m/z = 146) and P11 (m/z = 116) are formed by ring opening and demethylation. Eventually, the smaller organic molecular intermediates P5, P6, P10, and P11 are mineralized into H<sub>2</sub>O and CO<sub>2</sub> [71].

# 3.4. Fenton-like degradation mechanism of TC

To further investigate the mechanism of Fenton-like catalytic reactions, the active free radicals produced in the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub> system were explored by quenching experiments. In the Fenton-like process, hydroxyl radicals ( $\bullet$ OH) and superoxide radicals ( $\bullet$ O<sub>2</sub>) are generally considered to be the active species. Tert-butanol (TBA) and pbenzoquinone (BQ) were selected as quenchers of  $\bullet$ OH and  $\bullet$ O<sub>2</sub>, respectively [72]. As shown in Fig. 9, with the addition of BQ, the degradation effect of TC was slightly inhibited, indicating that  $\bullet$ O<sub>2</sub> may not be important in TC degradation. In contrast, the degradation of TC was significantly inhibited after adding TBA, which indicated that  $\bullet$ OH played a major role in the degradation of TC.

The production of •OH and •O<sub>2</sub> radicals by aqueous H<sub>2</sub>O<sub>2</sub> in the presence or absence of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE was examined by electron spin spectroscopy (ESR) using DMPO free radical capturing agent. When only an aqueous H<sub>2</sub>O<sub>2</sub> solution was used no ESR signals corresponding to •OH or •O<sub>2</sub> can be detected. However, when Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is introduced into the H<sub>2</sub>O<sub>2</sub> solution, the ESR signals corresponding to both •OH and •O<sub>2</sub> can be detected (Fig. 10. a and b). Accordingly, a postulated TC degradation by H<sub>2</sub>O<sub>2</sub> in the presence of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is presented.

According to the experimental results so far presented, the possible reaction mechanism of TC degradation by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub> is proposed as shown in Fig. 11. Under acidic conditions, Fe<sup>3+</sup> and Cu<sup>2+</sup> present in Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE react with H<sub>2</sub>O<sub>2</sub> to form Fe<sup>2+</sup> and Cu<sup>+</sup> (Eqs. (1) and (2)) [73]. The Fe<sup>2+</sup> and Cu<sup>+</sup> then further react with H<sub>2</sub>O<sub>2</sub> to generate •OH by Fe<sup>2+</sup>  $\rightarrow$  Fe<sup>3+</sup> and Cu<sup>+</sup>  $\rightarrow$ Cu<sup>2+</sup>conversion in a cyclic fashion (Eqs. (3) and (4)) [74]. At the same time, some portion of Fe<sup>3+</sup> reacts with •O<sub>2</sub>H to form •O<sub>2</sub> (Eq. (5)). In addition, Cu<sup>0</sup> and Cu<sup>+</sup> in Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE can donate electrons to reduce Fe<sup>3+</sup>  $\rightarrow$  Fe<sup>2+</sup>, by Cu<sup>0</sup> and Cu<sup>+</sup> via a rapid conversion cycle (Eqs. (6) and (7)) [54,75]. According to the XPS data, the role of Cu<sup>0</sup> in reducing Fe<sup>3+</sup> to Fe<sup>2+</sup> is shown in postulating the proposed mechanism (Fig. 11). In summary, the synergy between Cu<sup>0</sup>/Cu<sup>2+</sup> and Fe<sup>2+</sup>/Fe<sup>3+</sup> cyclic conversion improves the catalytic performance of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE/H<sub>2</sub>O<sub>2</sub>.

$$Fe^{3+} + H_2O_2 \rightarrow Fe^{2+} + \bullet O_2H + H^+$$
 (1)

$$Cu2+ + H2O2 \rightarrow Cu+ + \bullet O2H + H+$$
(2)



Fig. 8. Proposed degradation pathways of TC in the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE Fenton-like system.



Fig. 9. (a) and (b) Effect of radical scavengers on the degradation of TC (Reaction conditions: pH 5.0; initial TC, 50 mg/L; catalyst, 200 mg/L; H<sub>2</sub>O<sub>2</sub>, 4.0 mM).



Fig. 10. ESR spectra of •OH (a) and  $\bullet O_2^-$  (b) generated by Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE.



Fig. 11. The Schematic diagram of TC degradation by  $Cu/CuFe_2O_4/DE$  composites in Fenton-like systems.

$$Fe^{2+} + H_2O_2 \rightarrow Fe^{3+} + \bullet O_2H + OH^-$$
 (3)

$$Cu^{+} + H_2O_2 \rightarrow Cu^{2+} + \bullet OH + OH^{-}$$
(4)

$$\operatorname{Fe}^{3+} + \bullet \operatorname{O}_{2} \operatorname{H} \to \operatorname{Fe}^{2+} + \bullet \operatorname{O}_{2}^{-} + \operatorname{H}^{+}$$
(5)

$$Cu^{+} + Fe^{3+} \rightarrow Fe^{2+} + Cu^{2+}$$
 (6)

$$Cu^{0} + 2Fe^{3+} \rightarrow 2Fe^{2+} + Cu^{2+}$$
 (7)

$$\bullet O_2^- / \bullet OH + TC \rightarrow CO_2 + H_2O$$
(8)

#### 3.5. Catalyst stability and reusability

The stability and reusability of the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite were determined by measuring its metal ion leaching propensity and the catalyst activity deterioration upon repeated use for TC degradation. As shown in Fig. 12(a), with the introduction of diatomite, the Cu<sup>2+</sup> and Fe<sup>2+</sup> leaching from Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE reduced significantly due to their surface complexing with  $\equiv$ SiOH sites on porous diatomite. In addition, the recyclability of the used catalyst on TC degradation was also investigated. Spinel-type CuFe<sub>2</sub>O<sub>4</sub> has strong magnetic properties. Fig. S6 shows the hysteresis loop of the Cu/CuFe<sub>2</sub>O<sub>4</sub> nanocomposite with an applied magnetic field of  $\pm 2$  T. After Cu/CuFe<sub>2</sub>O<sub>4</sub> loading onto diatomite, the intensity of saturation magnetization (Ms) of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE decreases slightly; however, the reduced magnetic



Fig. 12. (a) Leaching amount of copper and iron ions from catalyst; (b) Removal efficiency of TOC and TC. (Reaction conditions: pH 5.0; initial TC, 50 mg/L; catalyst, 200 mg/L; H<sub>2</sub>O<sub>2</sub>, 4.0 mM).

intensity is still adequate to separate spent particulates from the reaction mixture (Fig. S7). To explore the reusability of the spent Cu/CuFe<sub>2</sub>O<sub>4</sub>/ DE catalyst, the TC degradation experiments were also carried out under an identical experimental setup for five cycles. As shown in Fig. 12(b), after five cycles, the TC removal rate by spent Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is maintained at 80 %, and the TOC mineralization rate of TC is maintained at 66 %, showing its sustained reactivity. In conclusion, the results show that the Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composite has good stability and repeatability.

# 4. Conclusion

Presently, Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE composites, prepared by a one-step solvothermal method, were used as a heterogeneous Fenton-like catalyst to degrade TC under acidic conditions. The excellent catalytic performance of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE is due to its large specific surface area, better pore size distribution, and abundant surface-active sites. The degradation rate of Cu/CuFe<sub>2</sub>O<sub>4</sub>/DE remains above 80 % after 5 consecutive cycles, showing high stability and reusability. The diatomite carrier can not only solve the Cu/CuFe<sub>2</sub>O<sub>4</sub> agglomeration problem but also limit the leaching of metal ions in the catalyst, which is due to its complexation with the silica hydroxyl group and the pore limitation effect of diatomite. The introduction of  $Cu^0$  enhances the catalytic activity of the material, and the synergy between  $Cu^+/Cu^{2+}$  and  $Fe^{2+}/Fe^{3+}$  redox pairs enhanced the generation of free radicals required for TC degradation. Hydroxyl radical played a leading role in the degradation and removal of TC during the reaction. The work of this paper provides a new idea for the preparation of heterogeneous Fenton-like catalysts with high catalytic efficiency and good reuse by combining diatomite, Cu<sup>0</sup>, and CuFe<sub>2</sub>O<sub>4</sub>.

#### **CRediT** authorship contribution statement

Shuai Deng: Methodology, Validation, Writing – original draft, Funding acquisition; Zhi Guo: Methodology, Writing – review & editing; Yi-Han Chen: Methodology, Validation; Kang-Ping Cui: Methodology, Validation; Zhao-Gang Ding: Methodology, Writing – review & editing; Bei Wang: Methodology; Rohan Weerasooriya: Writing – review & editing; Xing Chen: Validation, Investigation, Writing – review & editing.

#### **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### Data availability

Data will be made available on request.

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# Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.jece.2023.110045.

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