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# Short communication

# Infrared light active photocatalyst for the purification of airborne indoor pollutants



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# K.M.S.D.B. Kulathunga, Asangi Gannoruwa, Jayasundera Bandara \*

National Institute of Fundamental Studies, Hantana Road, CP 20000 Kandy, Sri Lanka

## ARTICLE INFO

# ABSTRACT

borne pollutants found in indoors.

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## 1. Introduction

Airborne pollutants such as volatile organic compounds (VOC), hydrogen sulphide, nitrogen oxides, and carbon monoxide, can cause health problems. Among common organic pollutants, phenolic compounds are highly volatile and the VOCs are of particular concern in air pollution [1,2]. As airborne phenolic compounds have been especially recognized as carcinogenic agent for human, strict guidelines have been implemented to regulate the airborne phenolic compounds [3]. An extensive attention has been devoted to find efficient routs to destroy organic pollutant from air, water and soil. Advanced oxidative processes (AOP) have been applied successfully for the degradation of phenolic compounds.

AOP confine with chemical and physical agents such as a combination of oxidizing agents such as semiconductors/photocatalyst, hydrogen peroxide, ozone and electrochemical oxidation. In heterogeneous photocatalysis, phenolic compounds are broken down to smaller nontoxic compounds on the semiconductor materials with the assistance of UV and visible radiations [3,4]. The most widely used semiconductor photocatalyst i.e.  $TiO_2$  is photoactive in the higher energy range of solar spectrum due to high band gap of  $TiO_2$ . Therefore, bandgap engineering is essential for the tuning of bandgap energy of  $TiO_2$  in order to activate in lower energy radiations such as IR and visible regions of solar spectrum. Many attempts have been devoted to utilize the visible spectrum of solar energy by impurity doping, metallization and sensitization of  $TiO_2$  [5–8]. However, catalysts that utilize the IR region which confine over 47% of solar spectrum for the photodegradation of pollutants are rare. Finding IR and near IR active photocatalysts for the degradation of common indoor pollutants is of great interest as IR and near IR photons are the common radiations found in indoor conditions. In this study, utilization of IR region for the degradation of airborne pollutants by silver nanoparticle embedded TiO<sub>2</sub> photoactalyst is reported and the catalyst has great application in abatement of indoor airborne pollutants.

In photocatalysis, most of the catalysts area active either for UV or visible radiations and infrared active catalysts

are rare. In this investigation, Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst was synthesized and successfully applied for the degradation

of gaseous phenol under IR irradiation. As the photodegradation described in this report involves low energy IR

photons under ambient indoor conditions, the catalytic system can be applied for the degradation of common air-

# 2. Experimental

The Ag embedded TiO<sub>2</sub> photocatalyst was prepared by slightly modified method which is given in our previous publications [6,9]. In brief, the catalyst was synthesized by slowly adding a stoichiometric amount of 1.0 M NH<sub>4</sub>OH to solutions containing x mg of AgNO<sub>3</sub> (x = 25.0, 30.0, 35.0, 40.0, 45.0 mg, BDH, Analytical grade) and 100 mg of TiO<sub>2</sub> (P25, Degussa) in 5 ml of water. Vigorous stirring was maintained during addition of NH<sub>4</sub>OH to complete hydrolysis of AgNO<sub>3</sub> and the suspension was heated at 120 °C until a dry powder is formed and the resulting dry product was sintered at 180°C for 1 h. In order to compare the photocatalytic behaviour of pristine TiO<sub>2</sub> and AgNO<sub>3</sub> catalysts, the similar procedure was followed except the addition of AgNO<sub>3</sub> and TiO<sub>2</sub> respectively.

The photocatalytic reaction was carried out in a gas sealed glass tube (10 ml) in which 50 mg of catalyst was spread as a thin film on the wall of the vessel. The reaction system was sealed with a gas sealed septum, wrapped three times with Al foil to make sure a complete dark condition and 10 ml of ~200 ppm phenol gas was injected to the sealed reactor at 60  $^{\circ}$ C and irradiation was carried out with IR light source in a

<sup>\*</sup> Corresponding author. *E-mail addresses:* jayasundera@yahoo.com, bandaraj@ifs.ac.lk (J. Bandara).

darkroom. For uniform irradiation, 8 bulbs of IR illuminating LED  $(880 \text{ nm}, \emptyset 5 \text{ mm}, \text{light intensity } 3.2 \text{ mW cm}^{-2})$  were mounted around the flask. Control experiments were done using the same reactor setup separately in the presence of TiO<sub>2</sub>, Ag<sub>2</sub>O and without any catalyst under IR illumination. Dark controls were carried out in the same reactor with TiO<sub>2</sub>/Ag<sub>2</sub>O, TiO<sub>2</sub> and Ag<sub>2</sub>O without the IR light source. Gaseous products of the reactor system were analysed by gas chromatography (Shimadzu, GC-9AM, packed charcoal column) coupled with TCD and Ar as carrier gas. To measure CO<sub>2</sub> at low concentrations, a higher amount of gaseous were injected to GC and average value of five analysis were taken as a reading. For low Diffuse Reflectance Infrared Fourier Transform spectroscopy (DRIFT) measurements of the catalysts were carried out by using Thermo Nicolet 6700 FT-IR spectrometer coupled with smart iTR. Diffuse reflectance analysis and luminescence experiments were done using a Shimadzu 2450 UV-vis spectrophotometer and Shimadzu RF 5000 recording spectrofluorophotometer instruments respectively. TEM image of the catalyst is recorded by FEI Tecnai F-20, 200 kV instrument.

#### 3. Results and discussion

In an earlier publication, we reported the characterization of the catalyst by SEM, XRD, XPS and TEM [6,9]. According to our previous results, presence of anatase and rutile forms of TiO<sub>2</sub> together with cubic Ag<sub>2</sub>O, AgO and Ag<sup>0</sup> in the catalyst were confirmed by the X-ray diffraction analysis. Also, XPS results confirmed that the catalyst contains Ag<sup>+</sup>, Ag<sup>0</sup>, Ti<sup>3+</sup> and Ti<sup>4+</sup> oxidation states and hence the catalyst was labelled as Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> [6,9]. The TEM image of the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst is shown in Fig. 1 and the magnified TEM image of the  $Ag_2O/TiO_2$  catalyst is shown in Fig. S1 in SI. The presence and distribution of Ag, Ag<sub>2</sub>O over TiO<sub>2</sub> can be observed in dark colour spots having two different sizes in Fig. 1, while, the light colour spots represent the TiO<sub>2</sub> nanoparticles. The distribution of Ag and Ag<sub>2</sub>O particles over TiO<sub>2</sub> found to sporadic, however almost all TiO<sub>2</sub> particles are covered with Ag and Ag<sub>2</sub>O nanoparticles. As shown in Fig. S1, the particles with fringe widths of 0.24 nm confirms the presence of Ag<sub>2</sub>O while the particles with fringe width of 0.35 nm confirm the presence of TiO<sub>2</sub> anatase [101] lattice plane. The UV-vis diffuse reflectance spectrum of the Ag<sub>2</sub>O/TiO<sub>2</sub> catalyst is shown in Fig. 2. As demonstrated earlier and shown in Fig. 2, the Ag<sub>2</sub>O/TiO<sub>2</sub> catalyst absorbs light from UV region to near IR region due to presence of reduced  $Ti^{3+}$  states in Ag<sub>2</sub>O/TiO<sub>2</sub> catalyst. [6,9].



Fig. 1. TEM micrographs of Ag<sub>2</sub>O/TiO<sub>2</sub> catalyst.



Fig. 2. Diffuse reflectance spectrum of Ag<sub>2</sub>O/TiO<sub>2</sub> catalyst.

The CO<sub>2</sub> yields when the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst with different ratios (i.e. TiO<sub>2</sub>:AgNO<sub>3</sub> (w/w), [(A) 100:25, (B) 100:30, (C) 100:35, (D) 100:40, (E) 100:45]) were irradiated with IR photons in the presence of gaseous phenol (200 ppm) are shown in the Fig. 3. The inset in Fig. 3 shows the CO<sub>2</sub> yield under the same condition in the presence of TiO<sub>2</sub> and Ag<sub>2</sub>O/Ag alone. As shown in Fig. 3, when Ag<sub>2</sub>O/Ag/TiO<sub>2</sub>, catalyst coated reactor containing gaseous phenol were irradiated with IR photons, formation of CO<sub>2</sub> was clearly observed with Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> while negligible CO<sub>2</sub> was observed with TiO<sub>2</sub> and Ag<sub>2</sub>O/Ag alone. i.e. in the cases of Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> (TiO<sub>2</sub>/Ag<sub>2</sub>O w/w ratio of 100:35), 27.70 µmols of CO<sub>2</sub> were observed after 2 h of irradiation while for TiO<sub>2</sub> and Ag<sub>2</sub>O alone, 0.10 µmols and less than 0.10 µmols of CO<sub>2</sub> were observed respectively after 2 h irradiation when ~200 ppm gaseous phenol was irradiated with IR photons. Detectable CO<sub>2</sub> or any other gaseous products were not observed for dark control experiments, with Ag/ Ag<sub>2</sub>O catalyst or in the absence of catalyst with IR illumination indicating that the photodegradation of gaseous phenol by Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst occurs only with IR photons. From the CO<sub>2</sub> yield shown in Fig. 3, it can be deduced that 21% mineralization of 200 ppm of gaseous phenol with Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst, prepared with 100:35 weight ratio of TiO<sub>2</sub>:AgNO<sub>3</sub> in 120 min. While with TiO<sub>2</sub> and Ag<sub>2</sub>O alone, a negligible amount of phenol was mineralized. As shown in Fig. 3, the degradation of phenol is highly depended on the TiO<sub>2</sub>:Ag<sub>2</sub>NO<sub>3</sub> ratio where increase in the TiO<sub>2</sub>:Ag<sub>2</sub>NO<sub>3</sub> ratio increase the degradation rate and the highest efficiency was noted when the  $TiO_2$ :Ag<sub>2</sub>NO<sub>3</sub> ratio was 100:35 (w/w). Further increase in the ration resulted in decrease in the degradation



**Fig. 3.** Yield of  $CO_2$  under IR irradiation in the presence of 200 ppm gaseous phenol with  $Ag_2O/Ag/TiO_2$  catalyst prepared with the weight ratio of (a) 100:35, (b) 100:40, (c) 100:45, (d) 100:30, (e) 100:25 TiO\_2 to AgNO\_3.

rate. The dependence of the phenol degradation with the TiO<sub>2</sub>:Ag<sub>2</sub>NO<sub>3</sub> ratio is given in Fig. S2 in the supporting information.

For further confirmation, that the observed degradation of phenol with Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> in the presence of IR radiation is not due to thermal activity, we investigated the thermal degradation of phenol at different temperatures without any catalyst or light. The Fig. S3 In SI shows the CO<sub>2</sub> yield with the reaction temperature in the presence of phenol with the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst and without any catalyst. As shown in Fig. S3, a considerable CO<sub>2</sub> amount was not noted up to 80 °C and from 80 °C onwards, the CO<sub>2</sub> production is gradually increased up to 210 °C and beyond this temperature a dramatic CO<sub>2</sub> yield is noted with the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst while at any temperature up to 250 °C, a considerable CO<sub>2</sub> amount was not noted in the absence of catalyst. These results indicate that phenol undergoes thermal oxidation at ~250 °C yet the amount CO<sub>2</sub> produced under thermal degradation (2.5 µmols) is much lower than the CO<sub>2</sub> produced under photodegradation (30 µmols). These results undoubtedly confirm that the origin of observed CO<sub>2</sub> was due to photodegradation of gaseous phenol by Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst with IR photons and not due to thermal degradation of phenol.

The degradation results presented indicated that the degradation of gaseous phenol occurred only with Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst while both TiO<sub>2</sub> and Ag<sub>2</sub>O alone showed a little or a negligible catalytic activity with IR photons. Hence, for the verification of these results, phenol adsorption and degradation on TiO<sub>2</sub> and Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> under IR illumination were analysed using FTIR spectroscopy and the results are shown in Fig. 4A and B respectively. In Fig. 4A, the broad peaks at about 3356 and 1642 cm<sup>-1</sup> correspond to the surface-adsorbed water and hydroxyl groups of TiO<sub>2</sub> respectively and a feeble peak at  $850 \text{ cm}^{-1}$  corresponds to the Ti-O-Ti stretching vibration of Ti ions in an octahedral coordination (spectrum a in Fig. 4A) [10–14]. The spectrum A2, in Fig. 4A shows the vibrational spectra of adsorbed phenol on TiO<sub>2</sub>. For the adsorbed phenol on TiO<sub>2</sub>, where bands located at 1595, 1499 and 1473 cm<sup>-1</sup> could be assigned to C=C stretching and C-H stretching vibrations [15–18]. While the band at 1368 cm<sup>-1</sup> corresponds to OH bending and the band located at  $1239 \text{ cm}^{-1}$  is due to stretching vibrational modes of C—O in the aromatic ring [16,17]. The spectra A3, A4 and A5 in Fig. 4A show the vibrational spectra of adsorbed phenol on TiO<sub>2</sub> with the IR irradiation time of 30, 90, and 120 min respectively. Careful analysis of spectra A3, A4 and A5 indicates that there are no significant changes in intensity of phenol vibrations despite 0.05% mineralisation of phenol on TiO<sub>2</sub>. These results confirm that the TiO<sub>2</sub> itself is a rather inactive photocatalyst with IR irradiation.

Similarly, phenol adsorption and degradation on Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> is demonstrated in Fig. 4B. Compared to broad vibrational spectra observed for surface-adsorbed water and hydroxyl groups of bare TiO<sub>2</sub>, for bare Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst, four bands were observed at 3053, 3196, 3273 and 3356 cm<sup>-1</sup> which are associated with the presence of hydroxyl groups [17]. In the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> bare catalyst, the band at 1633 cm<sup>-1</sup> could be assigned to both hydroxyl groups of TiO<sub>2</sub> (Ti—OH) and Ag—O vibrations [10,19]. Additional vibrational peaks were seen for  $Ag_2O/Ag/TiO_2$  bare catalyst in the range 1500–1200 cm<sup>-1</sup> (peaks at 1431, 1373, 1327 and 1219 cm<sup>-1</sup>) which are not seen in bare TiO<sub>2</sub> indicating those peaks are due to incorporation of Ag<sub>2</sub>O/Ag on TiO<sub>2</sub> and could be due to Brönsted and Lewis acid sites [20,21]. The characteristic vibrational peaks for adsorbed phenol are seen at 1585, 1489, 1470 cm<sup>-1</sup> (aromatic skeleton vibration plus C-H stretching), 1368 cm<sup>-1</sup> (OH bending), 1231 cm<sup>-1</sup> (stretching vibrational modes of C—O), 1167.5, 1050 and 1068 cm<sup>-1</sup> (C—H in plane bending), 996 and 977 cm<sup>-1</sup> (C—H out of plane bending) [18]. As shown in spectra of B3 and B4 in Fig. 5B, upon application of IR light for 30 and 90 min respectively, a progressive loss in the intensity of the original phenol vibrational peaks could be observed and after 120 min irradiation, phenol vibrational peaks have been totally disappeared justifying that the phenol undergoes degradation with IR photons in the presence of Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst.



**Fig. 4.** (A); The FTIR transmittance spectra of 'A1' pure TiO<sub>2</sub>, 'A2' after dark adsorption of phenol on TiO<sub>2</sub>, 'A3, A4, A5' are after 30, 90 and 120 min IR illumination of adsorbed phenol on TiO<sub>2</sub> respectively. 4(B); The FTIR transmittance spectra of 'B1' pure catalyst, 'B2' after dark adsorption of phenol 'B3,B4,B5' are after 30, 90 and 120 min IR illumination of adsorbed phenol on TiO<sub>2</sub> respectively.



Fig. 5. Schematic diagram of proposed photocatalytic process of Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst.

Surface analysis results together with degradation results indicated the IR initiated photodegradation of phenol on Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst and phenol is mineralized producing CO<sub>2</sub> during degradation. Characterization of catalyst has been reported in earlier publications, where it was shown that the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst consists of both Ag<sup>0</sup>/Ag<sup>+</sup> and Ti<sup>3+</sup>/Ti<sup>4+</sup> states in Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst. Photochemical water splitting reaction has been reported for the same catalyst and considering the excitation wavelengths of IR source (~850 and 950 nm) and the bandgap energies of TiO<sub>2</sub> (3.2 eV) and Ag<sub>2</sub>O (1.58 eV)/Ag, multiphoton excitation process where optical near field (ONF) and phonon assisted reaction mechanism has been proposed and discussed in detail for the observed water splitting reaction [7].

In the proposed ONF-phonon assisted process, formation of electron hole pairs are generated via multiphoton excitation process and can be explained as follows [22] even though phonon excited states are present in semiconductors, light cannot be excited from the valence band (VB) to those phonon excited states as these excitations are electric-dipole forbidden. However, as the ONF generated at the nanostructures could excite the coherent phonon in nanoparticles and these excited coherent phonon together with ONF forms exciton-phonon-polariton quasi states as shown in Fig. 5. These quasi particles can excite the electrons to the phonon level and successively to the CB. This type of multi-step excitation process is possible even the incident photon energy is lower than the band gap energy. The generation of ONF is a pre-requisite for the proposed e-h pair generation and as explained earlier, Ag<sup>0</sup> and Ag<sub>2</sub>O can generate phonons as well as ONF upon IR illumination as they are well known to generate plasmon as well as ONF [23–27].

Considering all these observations, a multiphoton process can be proposed for the observed photodegradation of gaseous phenol on Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst by IR photons where it involves filling of subband gaps in Ag<sub>2</sub>O and TiO<sub>2</sub> by trapping and de-trapping of electrons and holes created by IR photon excitation [6,9,22]. The proposed multiphoton process is schematically shown in Fig. 5 and the possible phenol degradation paths are given in reactions (1) to (5) [9,28]. To confirm the multiphoton process, we investigated the luminescence spectrum of Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst. As shown in Fig. 6, when the Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst is excited with 650 nm wavelength, a broad emission from 350 to 500 nm range with a maximum emission at ~458 nm was observed.

As given in reactions (1) to (5), once the e-h pairs are generated by multistep processes, excited electron react with oxygen to form oxygen radical holes form hydroxyl radicals. Both these radicals can degrade phenol by the reactions given in (4) and (5).

$$Ag_2O/TiO_2 + h\nu(IR) \rightarrow Ag_2O/TiO_2(e^- + h^+)$$
 (1)

$$Ag_2O/TiO_2(e^-) + O_2 \rightarrow Ag_2O/TiO_2 + O_2^{\bullet}$$
(2)



Fig. 6. Luminescence spectra of the catalyst  ${\rm Ag_2O/Ag/TiO_2}$  catalyst under excitation at 650 nm.

$$Ag_2O/TiO_2(h^+) + H_2O \rightarrow Ag_2O/TiO_2 + OH + H^+$$
(3)

$$C_6H_5OH_{(g)} + {}^{\bullet}OH + O_2 \rightarrow CO_2 + H_2O$$

$$(4)$$

$$O_2^{\bullet} + C_6 H_5 O H_{(g)} \rightarrow C O_2 + H^+$$
 (5)

#### 4. Conclusion

In conclusion, we have successfully demonstrated the IR initiated photodegradation of gaseous phenol on Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst. Phenol undergoes mineralization to produce CO<sub>2</sub> when the catalyst is irradiated with low energy IR photons. For the observed photocatalytic degradation of phenol by IR photons on Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> catalyst, a multiphoton excitation process was proposed. The Ag<sub>2</sub>O/Ag/TiO<sub>2</sub> photoactalyst is especially useful for the abatement of airborne pollutant in indoor conditions.

#### **Conflict of interest**

The authors declare that they have no conflict of interest.

#### Appendix A. Supplementary data

Supplementary data to this article can be found online at http://dx. doi.org/10.1016/j.catcom.2016.07.025.

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